

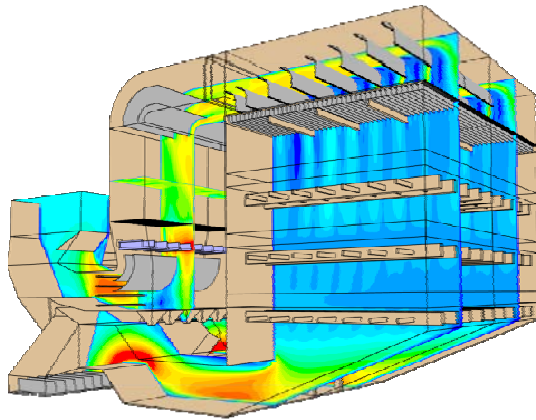
# **REINHOLD ENVIRONMENTAL Ltd.**



## **2012 NO<sub>x</sub>-Combustion Round Table & Expo Presentation**

February 13-14, 2012, in Columbus, OH / Hosted by AEP

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# SCR Gas Flow Modeling

Presentation for

Reinhold Environmental

2012 NOx Combustion Round Table

Columbus, OH

February 14, 2012

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# Overview

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- SCR Flow Modeling Methods
- Pros and Cons
- Typical Objectives and Techniques
- Model Accuracy
- Flow Visualization
- Conclusions
- Q&A

# *The Need for Flow Modeling...*

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- ❑ Performance Optimization
  - Flow Distribution...Ash Distribution
  - NH<sub>3</sub>/NO<sub>x</sub> Mixing/Distribution
  - Thermal Mixing
- ❑ O&M
  - Pressure Drop
  - Ash Accumulation
  - LPA Screen Capture
  - Erosion

# *The Need for Flow Modeling...*

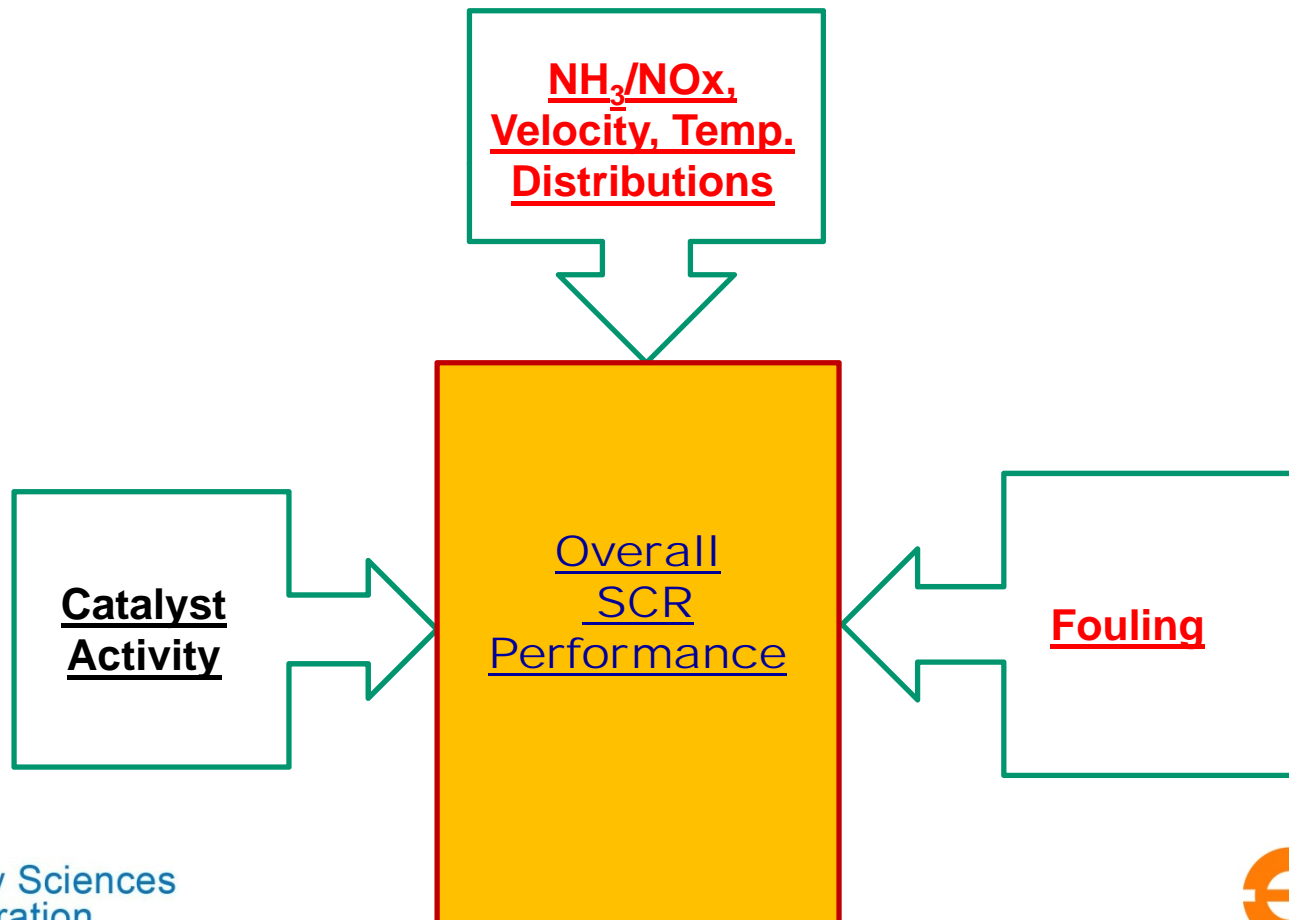
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- ❑ Trial and Error without modeling can work but...
  - Fixes can be costly
  - Results not as expected
  - New problems could develop
- ❑ Modeling can save time and \$\$ in the long run
- ❑ Can directly impact Catalyst Management
  - Poor distribution and/or ash buildup in reactor can significantly alter catalyst management strategies



# The Need for Flow Modeling...

**CATALYST ACTIVITY IS ONLY ONE PIECE OF THE PUZZLE !**



# *SCR Modeling...Physical & CFD*

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## □ Physical Modeling

- Utilizes a scale model (plexiglas)
- Geometrically identical to full-scale
- Ambient air as test gas
- Flow visualization
- Ash deposition
- Two-fluid mixing
- Allows for accurate simulations of complex phenomena



Typical 1/12 scale  
physical model

Turning vanes

AIG w/static mixers

Economizer bypass

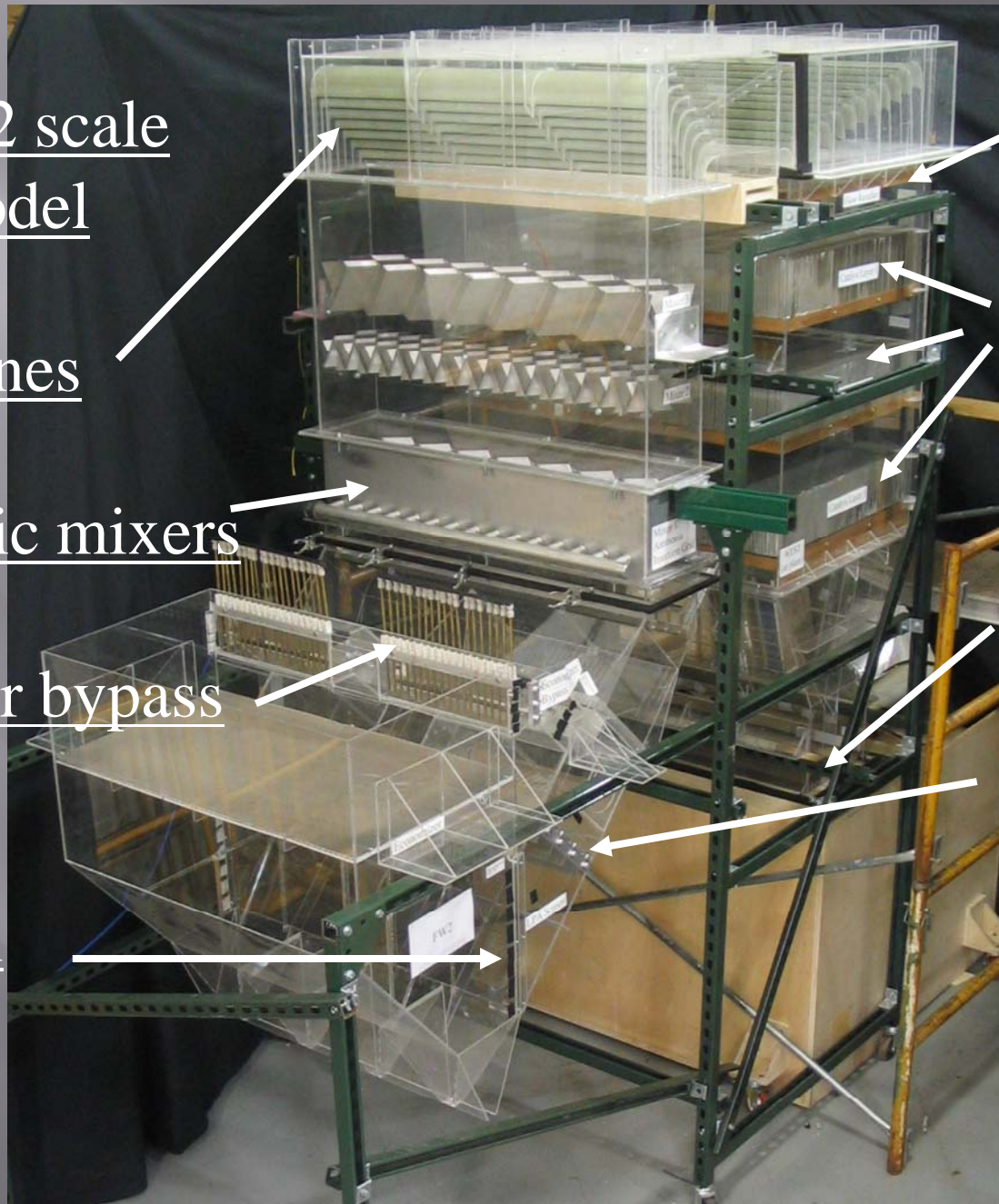
LPA screen

Rectifier

Catalyst  
layers

Air heater

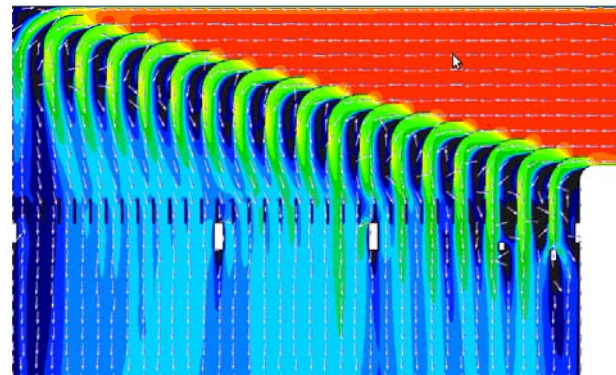
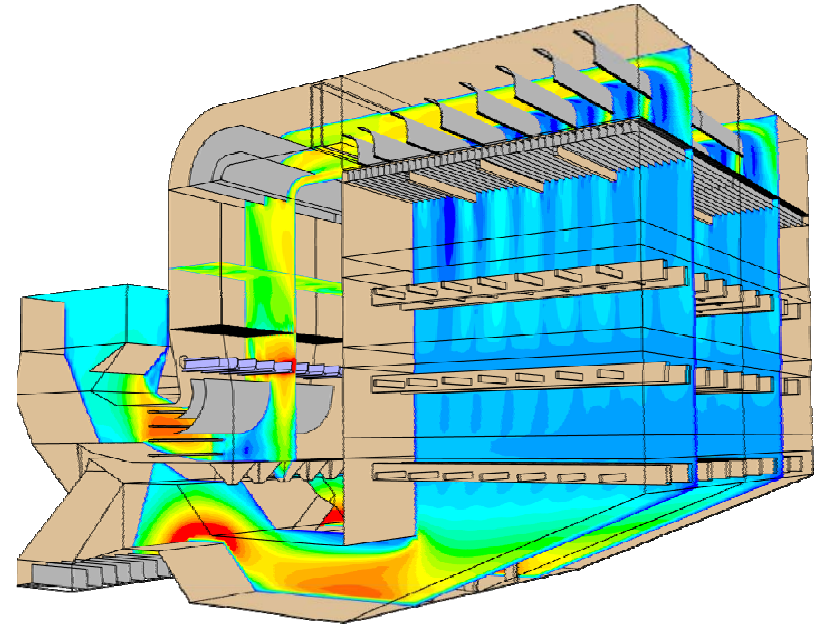
Dampers



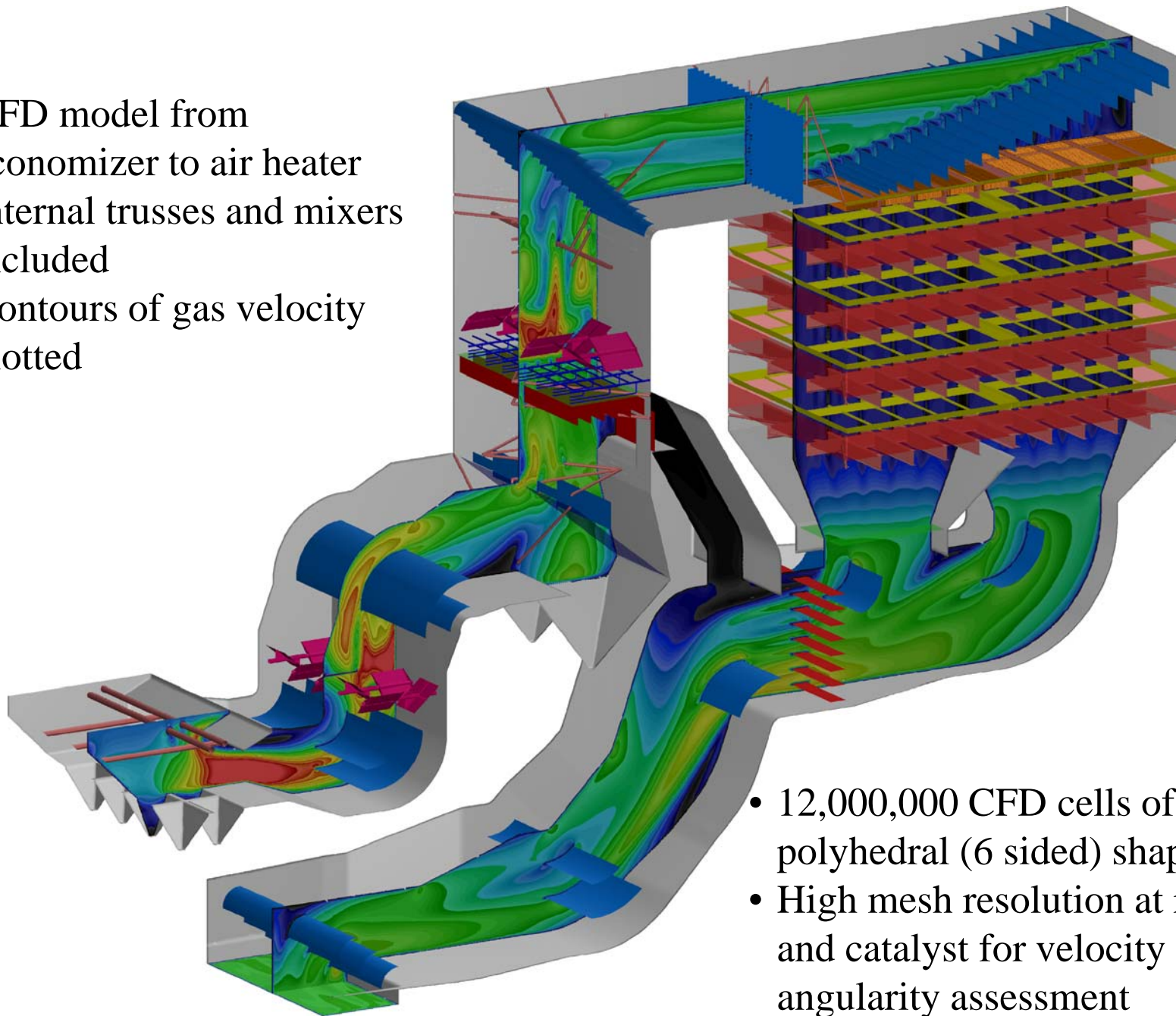
# *SCR Modeling...Physical & CFD*

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- ❑ Computational Fluid Dynamics (CFD)
  - Numerical simulation
  - All predictions performed with high-speed computers
  - Full-scale conditions
  - Complex geometries can be modeled
  - Detailed outputs



- CFD model from economizer to air heater
- Internal trusses and mixers included
- Contours of gas velocity plotted



- 12,000,000 CFD cells of primarily polyhedral (6 sided) shape
- High mesh resolution at rectifier and catalyst for velocity and angularity assessment

# *Physical & CFD...Pros and Cons*

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- ❑ Physical Modeling - Pros
  - Proven Technique
  - Complex flow simulations and solutions
  - NH<sub>3</sub> distribution modeling
  - Ash dropout / re-entrainment
  - Visualization
- ❑ Physical Modeling - Cons
  - Iterations can be time consuming
  - Thermal mixing difficult
  - Measurement points limited

# *Physical & CFD...Pros and Cons*

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- ❑ CFD Modeling - Pros
  - Iterations can be done quickly\*
  - Detailed representation of flow and mixing patterns
  - “Infinite” number of test points
  - Output can be very informative
  - Can track particulate in flight
- ❑ CFD Modeling - Cons
  - \* Large and complex models can be time consuming
  - Particulate dropout/re-entrainment modeling limited
  - NH<sub>3</sub> distribution modeling requires detailed mesh

# *Typical Modeling Objectives*

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- NH<sub>3</sub>/NO<sub>x</sub> Distribution
- Velocity Distribution
  - AIG Inlet
  - Catalyst Inlet/Outlet
  - Angularity at Catalyst
- Thermal Mixing
- Minimize Ash Buildup on Horizontal Surfaces
- Minimize Pressure Drop
- Optimize LPA Capture



# *SCR Ammonia Injection*

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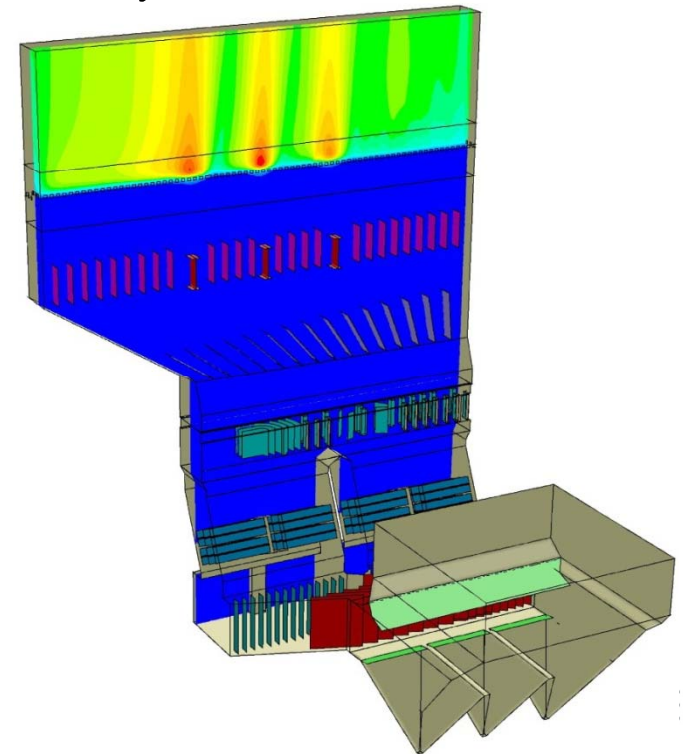
## ❑ Physical model

- Tracer gas injection
- Measure concentration gradient at catalyst



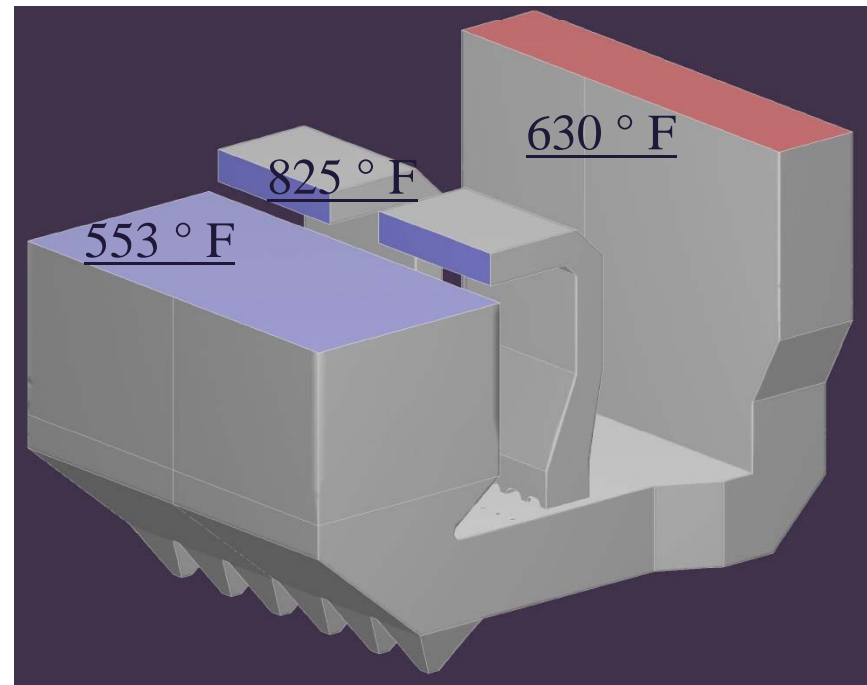
## ❑ CFD model

- Gaseous or liquid NH<sub>3</sub> injection
- Track species through ducts to the catalyst inlet



# SCR Thermal Mixing

- Economizer gas bypass used to boost SCR inlet gas temperature under low load operation
- Extract hot gas at econ inlet
- Inject into cooler econ outlet stream
- Need to mix the flows smoothly to obtain uniform temperature at catalyst with minimum DP
- Sounds simple enough, but there are many options and competing design elements



Without mixer,  $\Delta T = \pm 83$  °F

With mixer,  $\Delta T = \pm 15$  °F

# *Ash Deposition*

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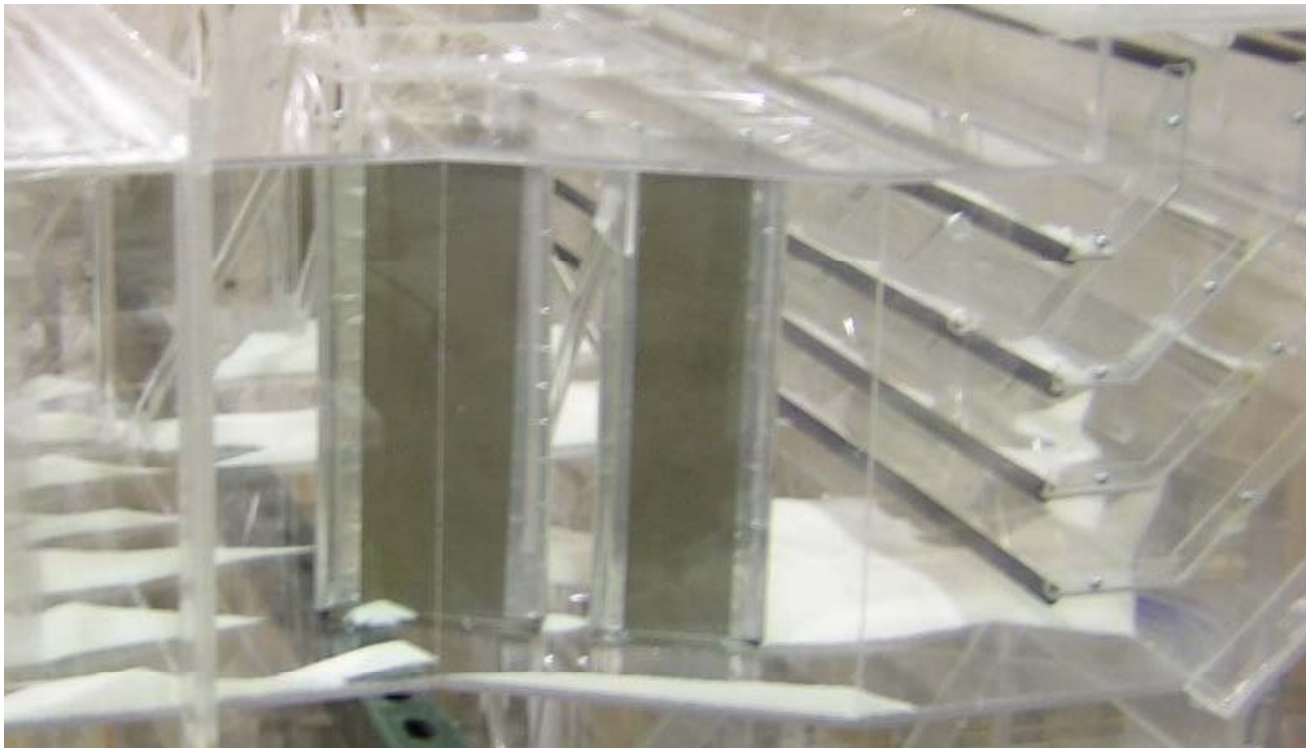
- Flues
- Turning vanes
- Catalyst



# *Ash Deposition – Model Testing*

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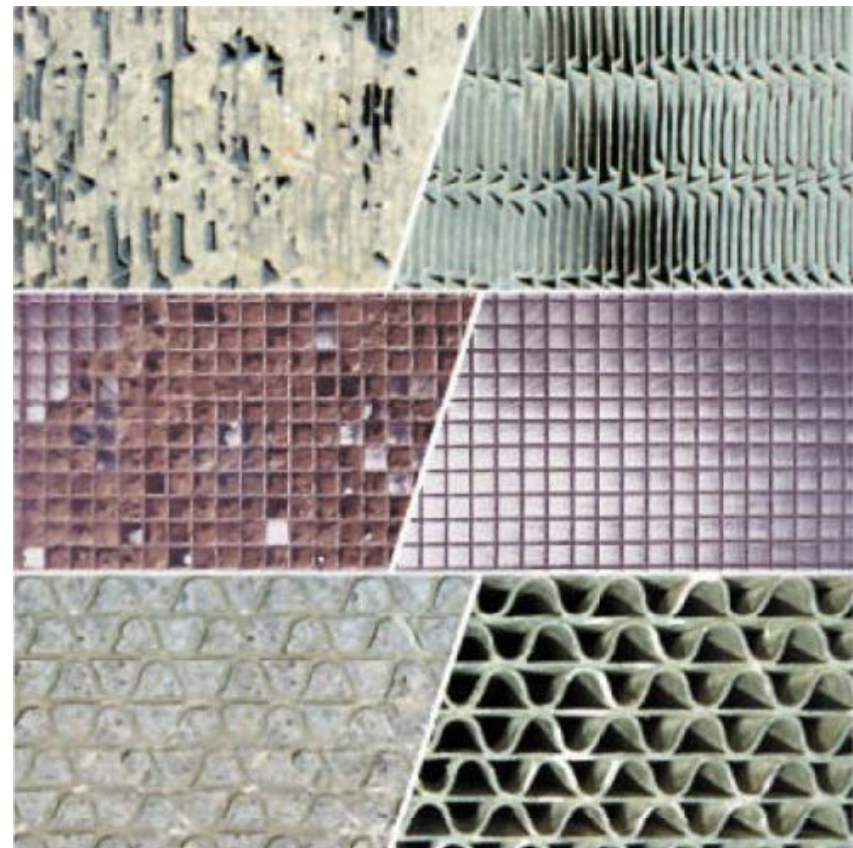
- Drop out
- Re-entrainment



# SCR Large Particle Ash

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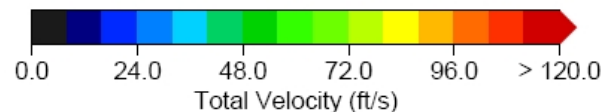
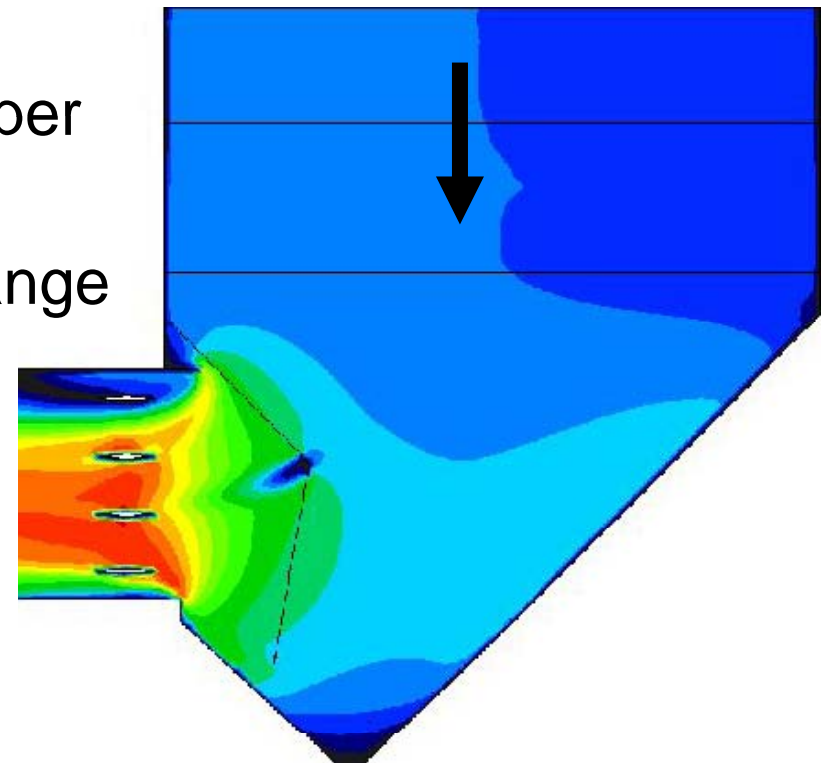
- ❑ SCR system design needs to effectively capture all LPA prior to the catalyst



# *LPA Modeling via CFD*

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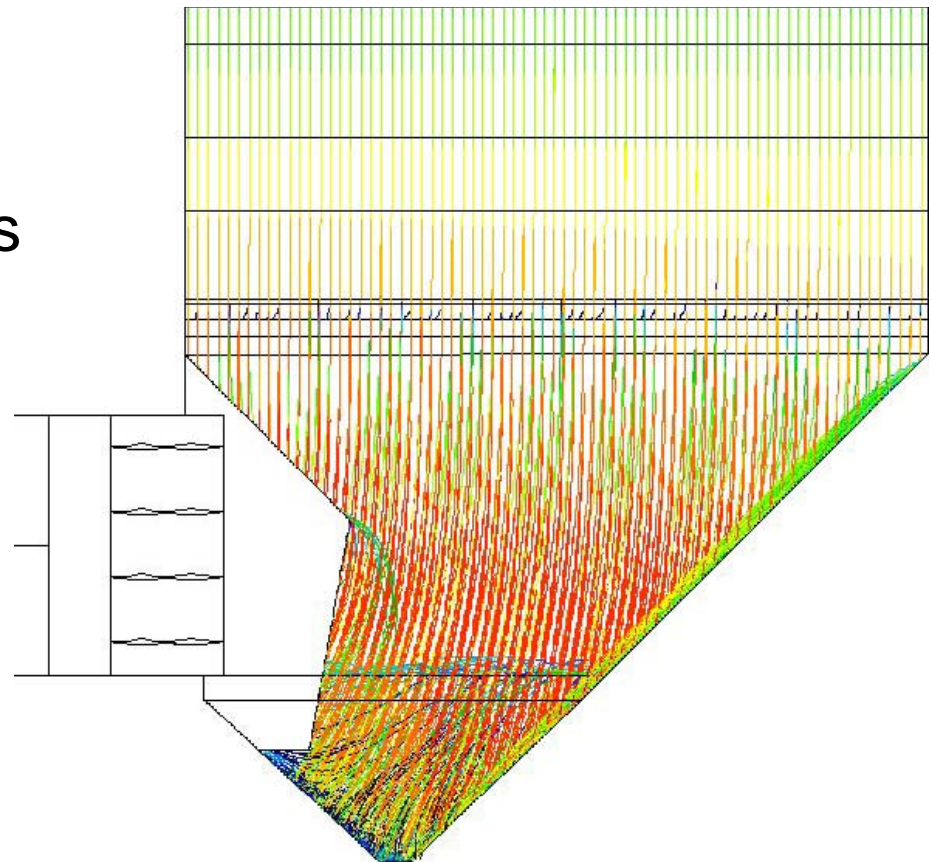
- Examine gas flow patterns and peak velocities through the system
- Track ash particles in flight through the ductwork and hopper regions
- Use model to evaluate wide range of design options



# *LPA Tracking*

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- Examine numerous particle sizes (3-7mm typical)
- Calculate particle paths
  - Rebound off surfaces
  - Impact on screen
  - Capture in hopper



# *LPA Modeling and Design – Key Points*

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- Ash capture statistics in hoppers
- LPA screen pluggage potential
- LPA screen erosion
- Pressure drop



# *Model Accuracy*

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- ❑ Do physical and CFD models match field test data?
  - Field data is unfortunately limited
  - Tend to go by industry experience and whether catalyst performance goals are met
- ❑ Do CFD and physical models match each other?
  - For velocity and pressure drop predictions, correlation is quite good
  - For NH<sub>3</sub> injection correlation has improved steadily over time
    - Better CFD meshes (= mesh quality and level of detail)
    - Faster computers (= larger CFD meshes)

# Model Comparisons – Velocity

Velocity at catalyst inlet (% RMS)				
Case	Load	Physical	CFD	Model Date
1	MCR	14.6	14.3	Jan-2007
1	70	13.5	14.3	Jan-2007
1	40	7.1	14.5	Jan-2007
2	Full	9.6	8.2	Oct-2007
3	100	10.7	5.8	Oct-2008
3	50	10.4	5.9	Oct-2008
3	40	8.6	5.7	Oct-2008
4	Full	10.2	11.4	Apr-2009
5	Full	9.5	9.3	Jul-2009
5	Mid	9	10.6	Jul-2009
5	Low	7.9	7.5	Jul-2009
6	100	7.9	7.2	Feb-2010
6	75	7.6	6.8	Feb-2010
6	37	7	6.5	Feb-2010

# Model Comparisons – Pressure Drop

DP (Inches of water, economizer to air heater)				
Case	Load	Physical	CFD	Model Date
1	MCR	4.2	5.1	Jan-2007
1	70	1.9	2.3	Jan-2007
1	40	1.3	1.4	Jan-2007
2	Full	6.9	7.3	Apr-2009
3	Full	9.6	10.1	Jul-2009
3	Mid	4.9	4.7	Jul-2009
3	Low	2.4	2.3	Jul-2009
4	100	5.6	5.8	Feb-2010
4	75	2.7	2.9	Feb-2010
4	37	1.3	1.3	Feb-2010

# Model Comparisons – NH<sub>3</sub> Distribution

NH3 at catalyst (% RMS)				
Case	Load	Physical	CFD	Model Date
1	MCR	2	5.1	Jan-2007
1	70	2.1	5.1	Jan-2007
1	40	8.6	9.5	Jan-2007
2	Full	3.1	5	Oct-2007
3	100	1.4	3.3	Oct-2008
4	Low	3.8	3.8	Jul-2009
5	100	2.2	3.1	Feb-2010
5	75	2.2	3.3	Feb-2010
5	37	2.4	3.4	Feb-2010

# *Flow Visualization*

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- Physical models – smoke flow, string tufts, dust injection/re-entrainment
- CFD models –animations of gas streamlines and particle pathlines

# *Flow Visualization - Physical*

- Video – Smoke flow

# *Flow Visualization - CFD*

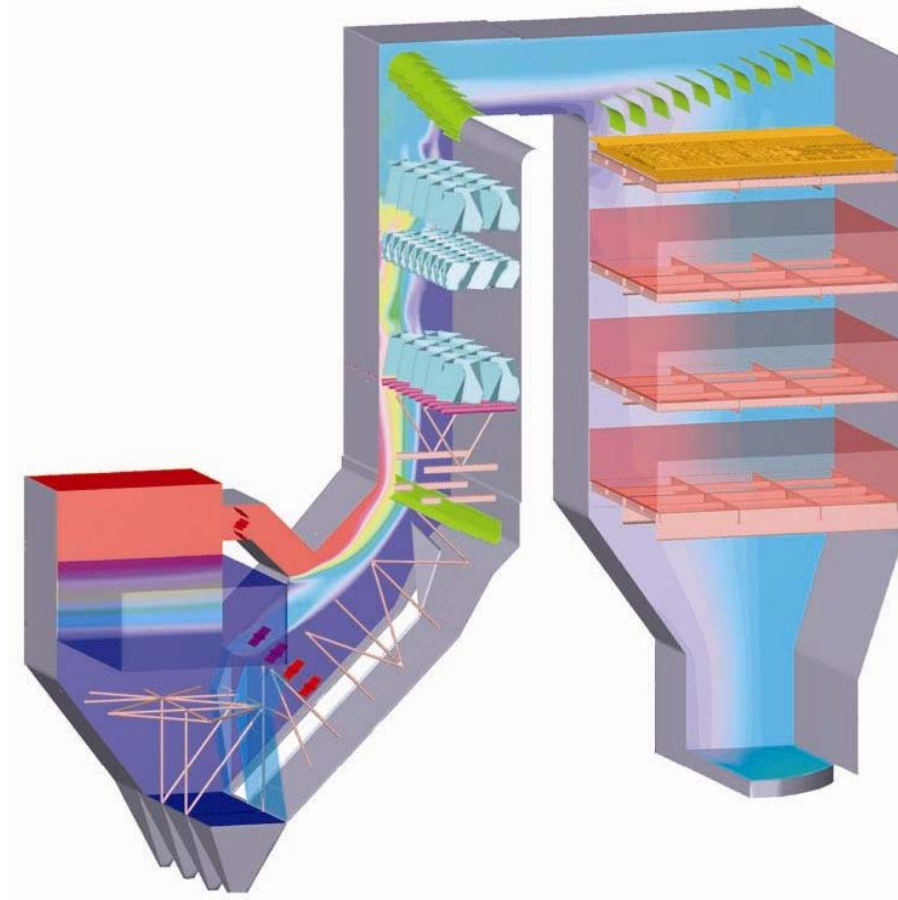
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- Video 1 – Streamline tracking

# *Flow Visualization - CFD*

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- Video 2 – SCR Fly Through



# *Conclusions*

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- Performance of SCR Systems relies heavily on flow conditions
- Analysis and design tools include physical and CFD flow modeling
- Both tools have their strengths, and can wisely be used to provide significant improvements and extend the life of catalyst

# Q&A

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